

Analysis of coupled heat transfer and thermal conductivity of fiber reinforced silica aerogel composite at high temperatures

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Introduction

In recent years, fiber reinforced aerogels have received extensive attentions. It is important to characterize the thermal conductivity of aerogels at high temperatures. However, the classic steady-state plate method can only obtain the apparent thermal conductivity of thick sample under large temperature difference. Due to semi-transparent radiation characteristics of fiber reinforced aerogel, the apparent thermal conductivity is affected by the internal skeleton heat conduction, gas molecule heat transfer and radiative heat transfer. Therefore, this paper will investigate the distribution of the apparent thermal conductivity under large temperature differences, and different pressure and high temperature conditions.

Model Establishment

For thick samples with large temperature differences, the correlation function between apparent thermal conductivity $\overline{\lambda}$ and actual thermal conductivity λ_{τ} is expressed as:

$$\overline{\lambda} = \int_{T_{\rm L}}^{T_{\rm H}} \lambda_T(T) dT / (T_{\rm H} - T_{\rm L})$$

where:

 $T_{\rm H}$ - hot side temperature, K;

 $T_{\rm L}$ - cold side temperature, K.

Based on Eq. (1), actual thermal conductivity λ_{τ} can be determined using the data of apparent thermal conductivities of samples at different hot surface temperatures.

Actual thermal conductivity λ_{τ} is relative to the solid-phase thermal conductivity, gas-phase thermal conductivity and radiative thermal conductivity of the aerogel. To decouple the thermal conductivity of each phase, the Rossland diffusion approximation is used to simplify the radiation transfer equation, an approximate formula for radiative thermal conductivity λ_{rad} was obtained [1]:

$$R_{rad} = \frac{16}{3\beta_R} n^2 \sigma T^3$$

where

 β_{R} - Rossland extinction coefficient, 1/m;

n - refractive index, -;

- σ Stefan–Boltzmann constant, W/m²K⁴;
- T absolute temperature, K.

For fiber reinforced aerogel with porosity of more than 90%, the gas-phase thermal conductivity can be expressed as using the modified Kaganer model [2]:

$$\mathbf{d}_{g} = \frac{(2.25\gamma - 1.25)0.461(p/k_{B}T)(8k_{B}T/\pi m_{g})^{V2}}{0.25S_{s}\rho_{\text{por}}\varphi^{-1} + \sqrt{2}(p/k_{B}T)\pi d_{g}^{2}} \frac{c_{v}}{N_{A}}$$

where:

- γ the ratio of specific heat capacity, -;
- *k*_{*B}</sub> Boltzmann constant, J/K;</sub>*
- *m_g* molecular mass, kg;
- s_s surface area per unit mass, m²/kg;
- $\rho_{\rm por}$ apparent density, kg/m³;
- φ porosity, -;
- d_s molecular diameter, m;
- c, molecular diameter, m;
- N₄- Avogadro constant, 1/mol.

The coupling of gas-phase thermal conductivity λ_s and solid-phase thermal conductivity λ_i is defined as gas-solid equivalent thermal conductivity $\lambda_{eff,sg}$. Based on the equivalent model proposed Maxwell-Garnett theory, $\lambda_{eff,sg}$ can be expressed as [3]:

$$\frac{\lambda_{eff,sg} - \lambda_g}{\lambda_{eff,sg} + 2\lambda_g} = \varphi \frac{\lambda_s - \lambda_g}{\lambda_s + 2\lambda_g}$$

Combining Eqs.(1)~(4), the actual thermal conductivity is expressed as :

 $\lambda_T = \lambda_{rad} + \lambda_{eff,sg}$

Results and Discussion

The apparent thermal conductivity of fiber reinforced silica aerogel sample under atmospheric pressure are shown in Tab. 1.

 Tab. 1. Test results of apparent thermal conductivity of fiber reinforced silica aerogel.

$T_{_{ m H}}$	TL	$\overline{\lambda}$
°C	°C	°C
20.4	200	0.0283
21.8	400	0.0382
24.2	600	0.0616
28.7	800	0.1044
32.6	900	0.1334

The spectral radiation properties are shown in Fig.1. The calculated results of thermal conductivities are shown in Fig.2.







Fig. 2. Decoupled results of thermal conductivity of each phase.

The solid-phase thermal conductivity changes greatly with the air pressure, which affects the apparent thermal conductivity. The actual thermal conductivities at different temperatures and pressures are shown in Fig.3. The predicted apparent thermal conductivities of the aerogel sample under different hot surface temperatures and pressures are shown in Fig.4.



Conclusions

In this paper, the conversion algorithm between apparent thermal conductivity and actual thermal conductivity of fiber reinforced aerogel was established. The Rossland diffusion approximation was used to describe the radiative thermal conductivity, and the modified Kaganer model was used to describe the gasphase thermal conductivity. Combined with the equivalent model proposed by Maxwell-Garnett theory, the actual thermal conductivity was successfully decoupled. Using the above models, the effects of temperature and pressure on the high-temperature apparent thermal conductivity of aerogel composites were discussed. This paper provides the data for the design and application of fiber reinforced aerogel.

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References

[1] T. Xie, Y. L. He, Z. J. Hu. Theoretical study on thermal conductivities of silica aerogel composite insulating material. International Journal of Heat and Mass Transfer 58, 540-552 (2013).

[2] S. Q. Zeng, A. Hunt, R. Greif. Mean free path and apparent thermal conductivity of a gas in a porous medium. Journal of Heat Transfer 117, 758-761 (1995).

[3] F. Garoosi. Presenting two new empirical models for calculating the effective dynamic viscosity and thermal conductivity of nanofluids. Powder Technology 366, 788-820 (2020).